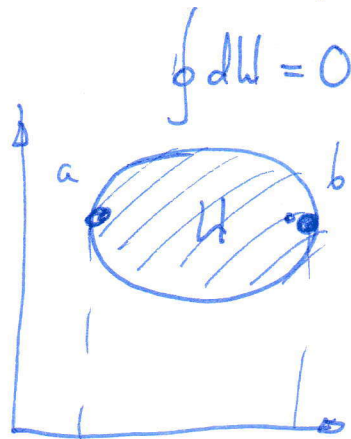
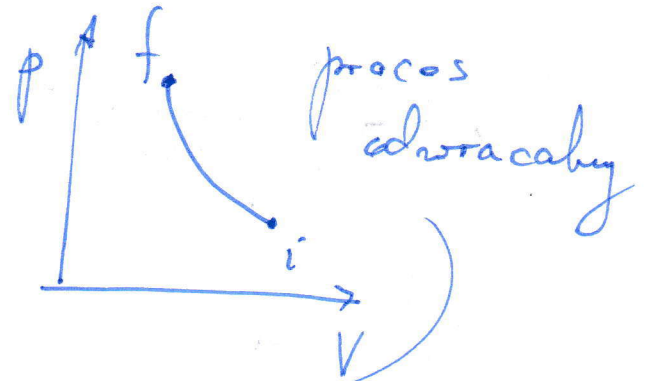
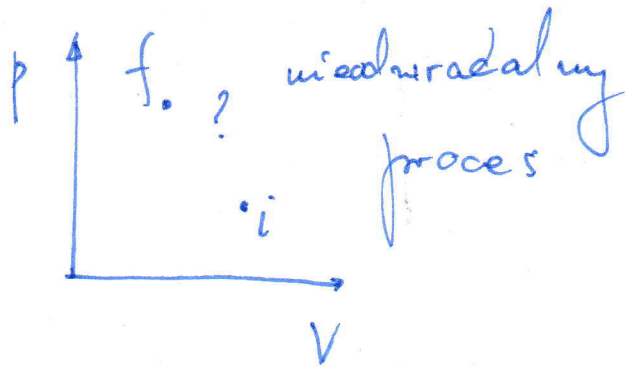


Entropia i II zasada TD



Za pomocą różniczkowej zmiany
stosunku można wywodzić p. odwracalny

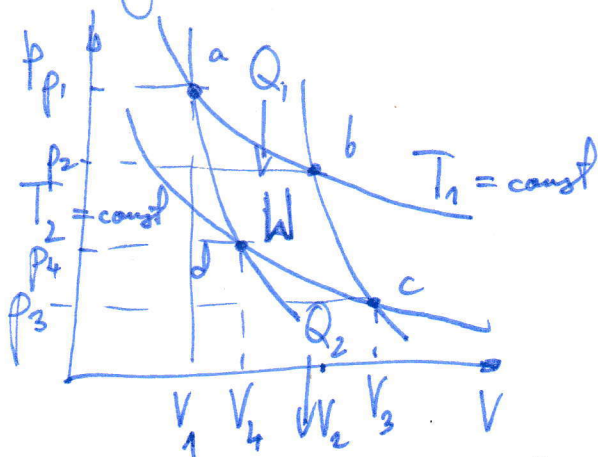
Silnik ciepły

$$W = Q_1 - Q_2$$

Sprawność

$$\eta = \frac{W}{Q_1} = 1 - \frac{Q_2}{Q_1}$$

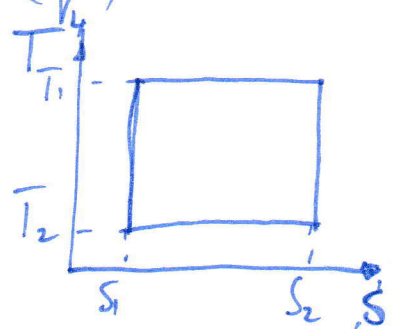
Cykl Carnota



$$Q_1 = W_1 = R T_1 \ln \left(\frac{V_2}{V_1} \right)$$

$$Q_2 = W_2 = R T_2 \ln \left(\frac{V_3}{V_4} \right)$$

$$\frac{Q_1}{Q_2} = \frac{T_1 \ln \frac{V_2}{V_1}}{T_2 \ln \frac{V_3}{V_4}}$$



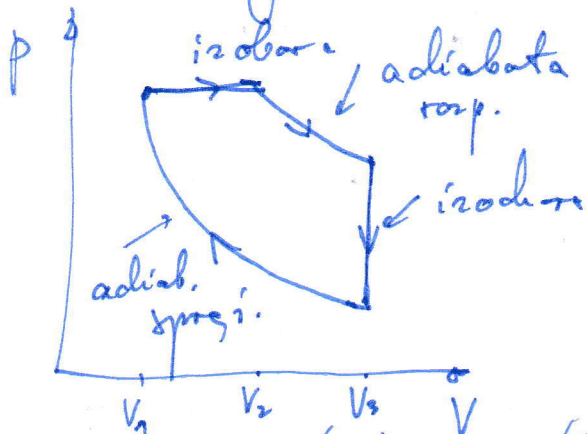
albo

$$\left. \begin{aligned} p_1 V_1 &= p_2 V_2 \\ p_3 V_3 &= p_4 V_4 \\ p_2 V_2^{\gamma} &= p_3 V_3^{\gamma} \\ p_4 V_4^{\gamma} &= p_1 V_1^{\gamma} \end{aligned} \right\} \Rightarrow \frac{V_2}{V_1} = \frac{V_3}{V_4}$$

coz

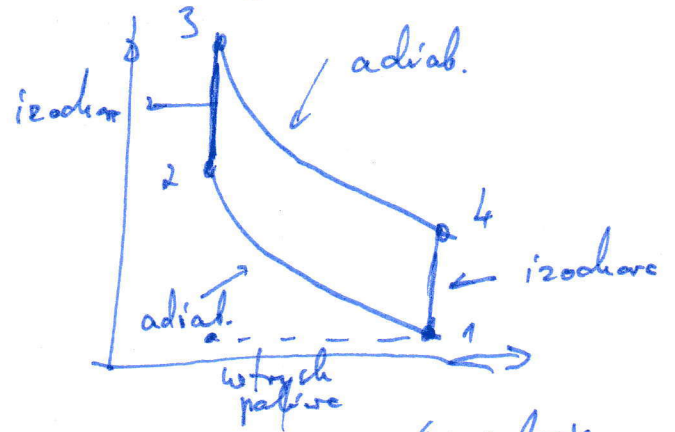
$$\eta = 1 - \frac{T_2}{T_1} = \frac{T_1 - T_2}{T_1}$$

Cykl Diesel



$$\eta = 1 - \frac{C_v}{C_p} \left(\frac{V_2}{V_3} \right)^{\gamma-1} \frac{1 - \left(\frac{V_1}{V_2} \right)^{\gamma}}{1 - \frac{V_1}{V_2}}$$

Cykl Otto

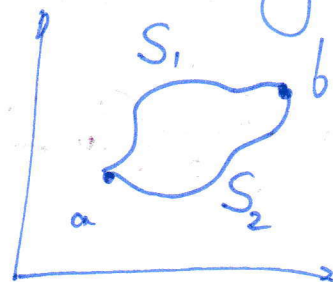


$$\eta = 1 - \left(\frac{V_1}{V_2} \right)^{\gamma-1}$$

Entropia #1

$$dS = \frac{dQ}{T} \quad \text{w procesach odwracalnych}$$

$$\oint dS = 0 \Rightarrow \int_a^b dS_1 + \int_b^a dS_2 = 0$$



Rozróżnienie procesów odwracalnych i nieodwracalnych
za pomocą entropii

II zasada TD

Procesy termodyn. przebiegają w takim kierunku
aby entropia nie zmalała

$$dS \geq 0$$

p. odwracalny
p. nieodwracalny

$$S_f = S_i$$

$$S_f > S_i$$

• Tępienie lodu

$$S_{\text{wody}} - S_{\text{lodu}} = \int \frac{dQ}{T} =$$

$$= \frac{Q}{T} = \frac{7.96 \times 10^4 \text{ cal}}{1220 \frac{\text{g}}{\text{K}}} =$$

• Rozprężanie $T = \text{const}$
gazu

$$dQ = p dV$$

$$dS = \frac{dQ}{T} = \frac{p dV}{T} \quad \text{ale } pV = RT$$

$$\int_i^f dS = R \int_{V_i}^{V_f} \frac{dV}{V} \Rightarrow S_f - S_i = R \ln \frac{V_f}{V_i} \quad (\text{entropia rośnie!})$$

Entropia

2

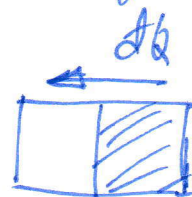
(miara nieporządku)

Def. statystyczna (Boltzmann) $S = -k_B \sum_i p_i \ln p_i$

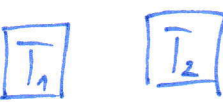
$$S = k_B \ln P$$

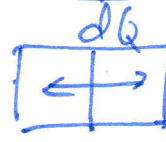
P - prawdopodobieństwo całkowite

$T_1 < T_2$  $\xrightarrow{\text{spontaniczne}}$



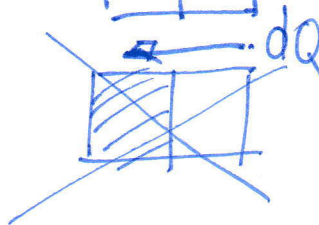
$$dS = dQ \left(\frac{1}{T_1} - \frac{1}{T_2} \right) > 0$$

$T_1 = T_2$  $\xrightarrow{\text{nie ma zmiany}}$



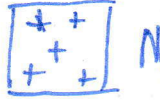
$$dS = dQ \left(\frac{1}{T_1} - \frac{1}{T_2} \right) = 0$$

$T_1 > T_2$  $\xrightarrow{\text{nie ma zmiany}}$



$$dS = dQ \left(\frac{1}{T_1} - \frac{1}{T_2} \right) < 0$$

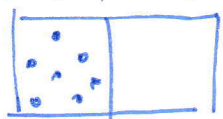
Entropia mieszania

S_1  N_1 S_2  $N_2 \Rightarrow S$  $N = N_1 + N_2$

$$\Delta S_m = S - (S_1 + S_2) = k_B N_1 \ln \frac{N}{N_1} + k_B N_2 \ln \frac{N}{N_2}$$

Rozprężanie gazu

N cząstek



$$P_1 = \left(\frac{1}{2} \right)^N$$

$$P_2 = 1 - \left(\frac{1}{2} \right)^N$$

$$\frac{P_1}{P_2} = \frac{\left(\frac{1}{2} \right)^N}{1 - \left(\frac{1}{2} \right)^N} \approx \left(\frac{1}{2} \right)^N$$

$$S_2 - S_1 = \Delta S =$$

$$k_B \ln P_2 - k_B \ln P_1 =$$

$$k_B \ln \frac{P_2}{P_1} = + k_B \ln 2^N$$

$$= k_B N \ln 2$$

Mamy rozkład kanonowy

$$Z = \sum_i e^{-\beta E_i}$$

$$\beta = (k_B T)^{-1}$$

funkcja rozkładu pozwala wyznaczyć
f. TD

$$U = \frac{\partial}{\partial \beta} (\ln Z)$$

energia wew.

Drugi rozkład kanonowy "ensemble"

$$Z^* = \sum_{i,n} e^{(-\beta E_i + \mu \beta n)} = \sum_{i,n} e^{+\beta(-E_i + n\mu)}$$

μ - potencjał chemiczny

$$F = -k_B T \ln Z$$

energia swobodna

zmienne termiczne

T, S

zmienne mechaniczne

p, V

Równowaga TD

$$\text{Jeśli } \begin{matrix} dT = 0 \\ dV = 0 \end{matrix} \Rightarrow F = F_{\min}$$

$$\text{Jeśli } \begin{matrix} dp = 0 \\ dQ = 0 \end{matrix} \Rightarrow H = H_{\min}$$

$$\text{Jeśli } \begin{matrix} dT = 0 \\ dp = 0 \end{matrix} \Rightarrow G = G_{\min}$$

Helmholtz

$$F = U - TS$$

$$H = U + pV$$

entalpia

Gibbs

$$G = U + pV - TS = F + pV =$$

entalpia swobodna

$$H - TS$$